



# The Impact of Duct Fitting Selection

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# Pat Brooks

Senior Project Manager, SMACNA

- Over 35 years experience in HVAC ductwork design and manufacturing
- Bachelor's & master's degrees in mechanical engineering, and masters' degree in business
- Member of ASHRAE and SPIDA technical committees on duct design; recently named ASHRAE Distinguished Lecturer





# **The Impact of Duct Fitting Selection**

## **Purpose and Learning Objectives**

The purpose of this presentation to help duct system designers learn how to calculate friction and dynamic losses as well as understand how the velocity and type of fitting impacts the design.

At the end of this presentation participants will be able to:

1. Explain how friction loss is calculated and how velocity affects the friction loss.
2. Explain fitting loss coefficients and how fitting losses are calculated.
3. Explain how the selection of a fitting affects the design leg of the duct system.
4. Describe how the size of ductwork or fitting selection can affect the system balance.

# SMACNA Manual

## HVAC SYSTEMS DUCT DESIGN

FOURTH EDITION – DECEMBER 2006

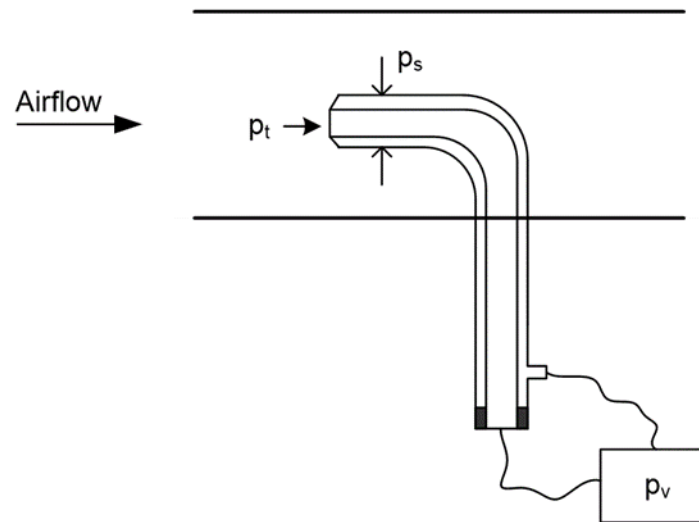


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# Pressure

$$p_t = p_s + p_v$$



Pitot-static tube

# Pressure - Changes in Pressure

$$\Delta p_t = \Delta p_s + \Delta p_v$$

Derived from the Bernoulli Equation:

$$p_{s1} + \frac{\rho_1 V_1^2}{2g_c} + \frac{g}{g_c} \rho_1 z_1 = p_{s2} + \frac{\rho_2 V_2^2}{2g_c} + \frac{g}{g_c} \rho_2 z_2 + \Delta p_{t,1-2}$$

# Pressure - Velocity Pressure ( $p_v$ )

$$p_v = \rho \left( \frac{V}{1097} \right)^2$$

Where:

$p_v$  = velocity pressure, in. of water

$V$  = velocity, ft/min

$\rho$  = density, lb<sub>m</sub>/ft<sup>3</sup>



# Pressure - Velocity Pressure ( $p_v$ )

$$p_v = \rho \left( \frac{V}{1097} \right)^2$$

Where:

$p_v$  = velocity pressure, in. of water

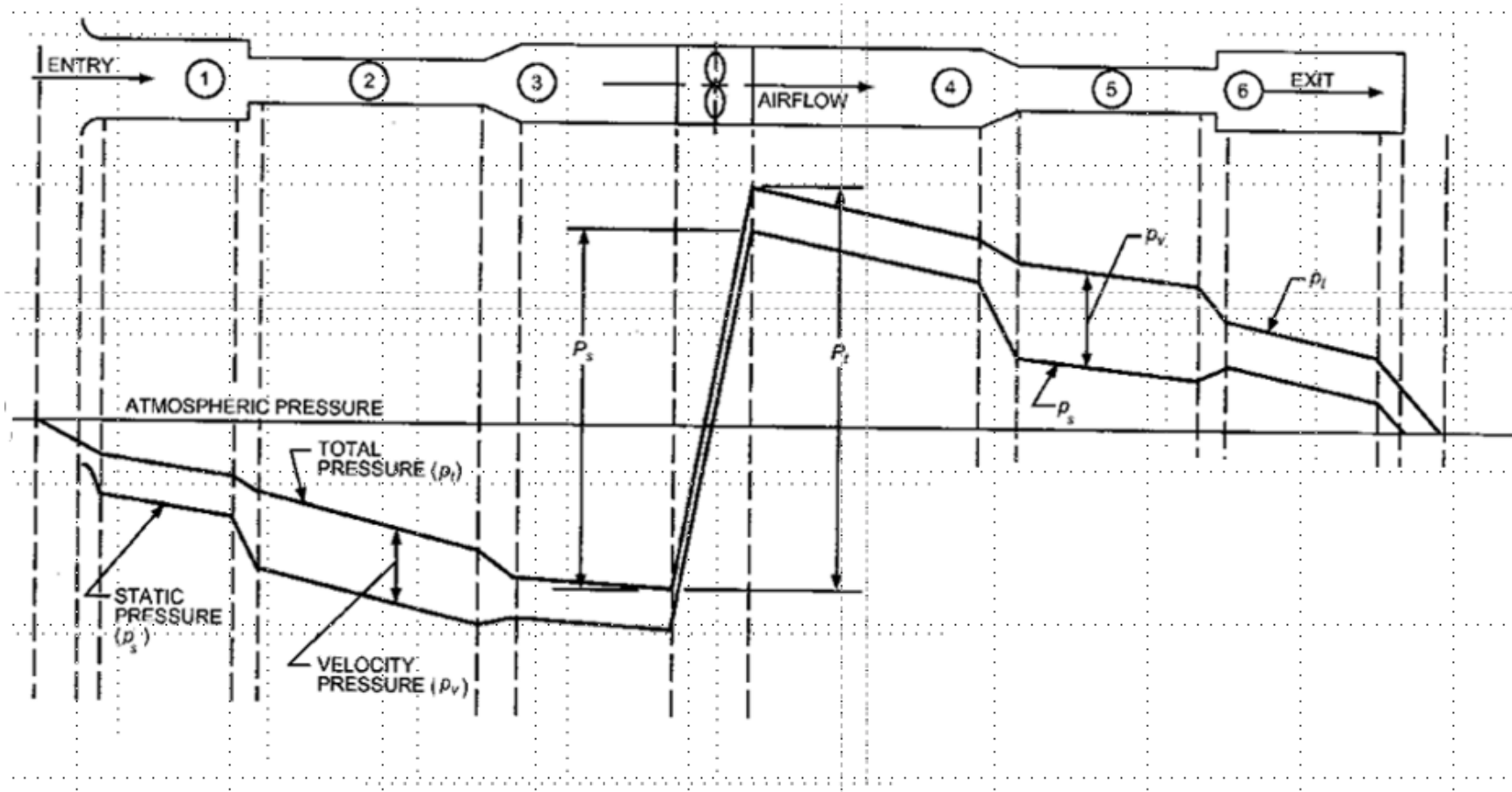
$V$  = velocity, ft/min

$\rho$  = density, lb<sub>m</sub>/ft<sup>3</sup>

$$p_v = \left( \frac{V}{4005} \right)^2 \text{ for standard air } \rho = 0.075 \text{ lb}_m/\text{ft}^3$$

# Pressure

## Pressure Changes During Flow in Ducts - Graphically



# Pressure Losses

- **Types**

- Friction Losses
- Dynamic Losses

# Pressure Losses

## Darcy-Weisbach Equation

$$\Delta p_t = \left( \frac{f L}{D_h} p_v \right) + \Sigma(C) * p_v$$

Where:

$f$  = friction factor

$L$  = Length, ft

$D_h$  = hydraulic diameter, ft

# Pressure Losses

## Friction – Darcy Equation

The left-hand side of the Darcy-Weisbach Equation is the Darcy Equation:

$$\Delta p_f = \left( \frac{f L}{D_h} p_v \right)$$



# Pressure Losses

## Friction – Colebrook Equation

$$\frac{1}{\sqrt{f}} = -2 \log \left( \frac{\varepsilon}{3.7 Dh} + \frac{2.51}{Re \sqrt{f}} \right)$$

The Colebrook equation was developed to calculate the friction factor,  $f$ ; requires you to also know the Reynolds Number,  $Re$ , and the absolute roughness,  $\varepsilon$  ( $ft$ ), which is determined experimentally.

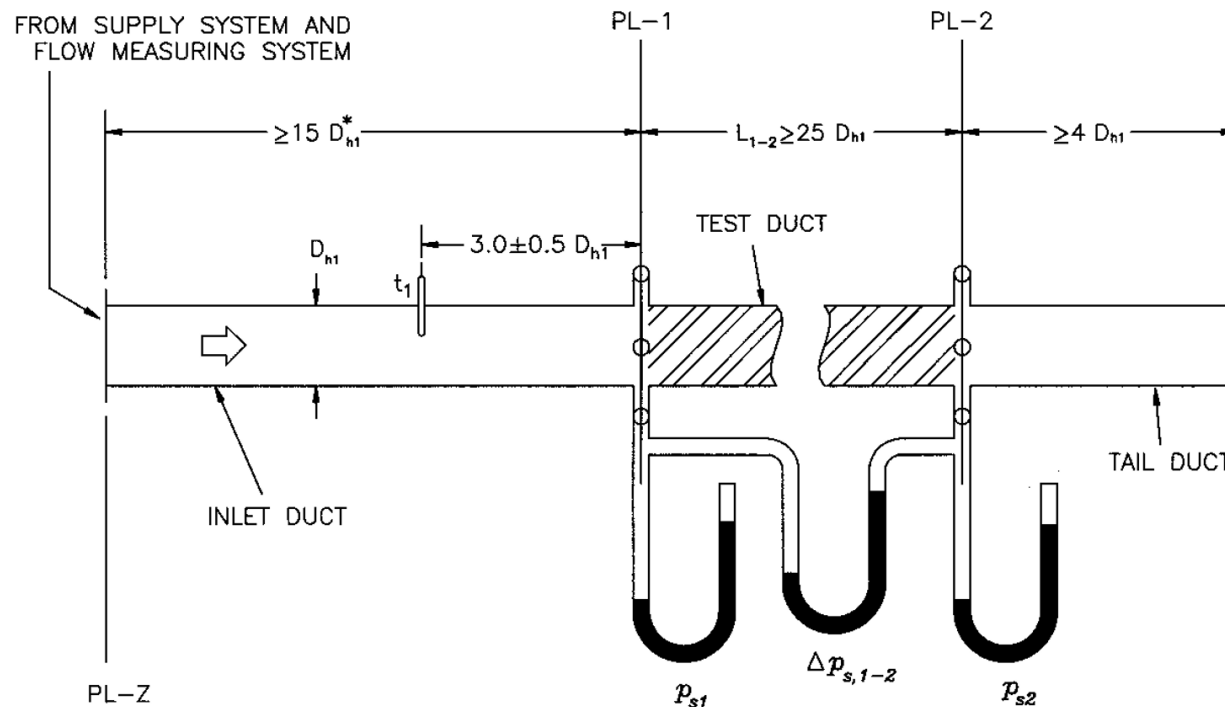
# Pressure Losses - Friction

Friction Losses are a function of the length, hydraulic diameter, the roughness of the material and the velocity pressure. Higher friction losses are caused by:

- Rougher Material (including joints)
- Longer Lengths
- Larger Velocity Pressures
- Smaller Diameters

# Pressure Losses

Friction – How Friction and Roughness Factors are determined



$$\Delta p_{f,1-2} = \frac{\Delta p_{s,1-2}}{L_{1-2}}$$

# Pressure Losses

## Friction – Colebrook Equation

**HVAC SYSTEMS DUCT**  
**Table A-1, pg A.4.**

Duct Material	Roughness Category	Absolute Roughness $\epsilon_1$	
		ft	mm
Uncoated carbon steel, clean (Moody 1944) (0.00015 ft) (0.05 mm) PVC plastic pipe (Swim 1982) (0.0003 to 0.00015 ft) (0.01 to 0.05 mm) Aluminum (Hutchinson 1953) (0.00015 to 0.0002 ft) (0.04 to 0.06 mm)	Smooth	0.0001	0.03
Galvanized steel, longitudinal seams, 4 ft (1200 mm) joints (Griggs 1987) (0.00016 to 0.00032 ft) (0.05 to 0.1 mm)	Medium Smooth	0.0003	0.09
Galvanized steel, spiral seam with 1, 2, and 3 ribs, 12 ft (3600 mm) joints (Jones 1979, Griggs 1987) (0.00018 to 0.00038 ft) (0.05 to 0.12 mm)	(New Duct Friction Loss Chart)		
Hot-dipped galvanized steel, longitudinal seams, 2.5 ft (760 mm) joints (Wright 1945) (0.0005 ft) (0.15 mm)	Old Average	0.0005	0.15
Fibrous glass duct, rigid Fibrous glass duct liner, air side with facing material (Swim 1978) (0.005 ft) (1.5 mm)	Medium Rough	0.003	0.9
Fibrous glass duct liner, air side spray coated (Swim 1978) (0.015 ft) (4.5 mm) Flexible duct, metallic, (0.004 to 0.007 ft (1.2 to 2.1 mm) when fully extended) Flexible duct, all types of fabric and wire (0.0035 to 0.015 ft (1.0 to 4.6 mm) when fully extended) Concrete (Moody 1944) (0.001 to 0.01 ft) (0.3 to 3.0 mm)	Rough	0.01	3.0

**Table A-1 Duct Material Roughness Factors**

# Pressure Losses

## Friction – Comparison of Different Velocities and Materials

**Example:** Calculate the Friction Loss in 100 ft of rectangular duct 24" x 32" at 1000 fpm, 2000 fpm, 3000 fpm and 4000 fpm for standard galvanized metal ( $\epsilon = 0.0003$  ft) and lined duct ( $\epsilon = 0.003$  ft)



# Pressure Losses – Friction

## Comparison of Different Velocities and Materials

Solution						
L =		100 ft				
Area =		5.33 ft <sup>2</sup>				
P =		9.33 ft				
D <sub>h</sub> =		2.29 ft				
$\rho = 0.075 \text{ lb}_m/\text{ft}^3$		Standard Conditions				
			Standard Galvanized ( $\epsilon = 0.0003 \text{ ft}$ )		Lined Duct, Corrugated Duct ( $\epsilon = 0.003 \text{ ft}$ )	
Velocity (fpm)	Velocity Pressure $p_v$ (inch water)	Q = AV Flow Rate (cfm)	Friction Factor, $f$	$\Delta p_f$ Friction Loss ( inch water)	Friction Factor, $f$	$\Delta p_f$ Friction Loss ( inch water)
1000	0.06	5333	0.0163	0.04	0.0220	0.06
2000	0.25	10667	0.0148	0.16	0.0215	0.23
3000	0.56	16000	0.0142	0.35	0.0213	0.52
4000	0.99	21333	0.0139	0.60	0.0212	0.92

# Pressure Losses

## Dynamic

The right-hand side of the Darcy-Weisbach Equation is the Weisbach Equation

$$\Delta p_{t, fittings} = \sum (C) * p_v$$

# Pressure Losses

Dynamic - How Loss Coefficients are Determined

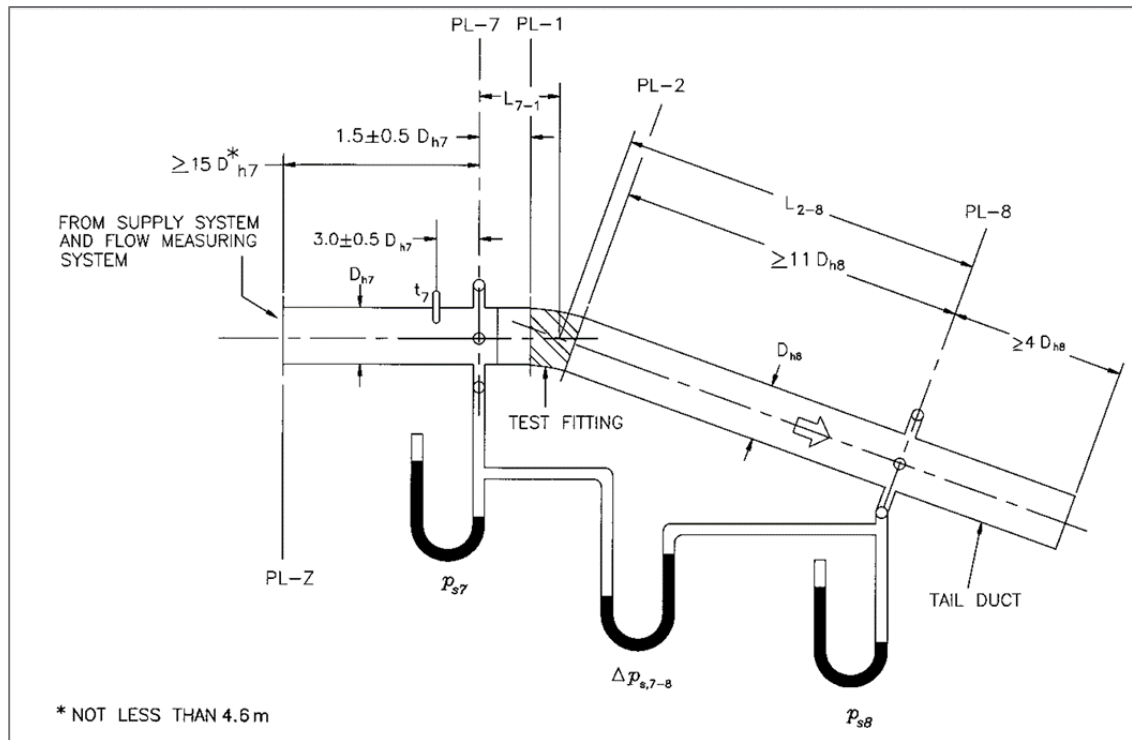
$$\Delta p_{t,fitting} = C * p_v$$

$$C = \frac{\Delta p_{t,fitting}}{p_v}$$

# Pressure Losses

## Dynamic – How Loss Coefficients are Determined

$$\Delta p_{t,fitting} = C * p_v, \quad C = \frac{\Delta p_{t,fitting}}{p_v}$$



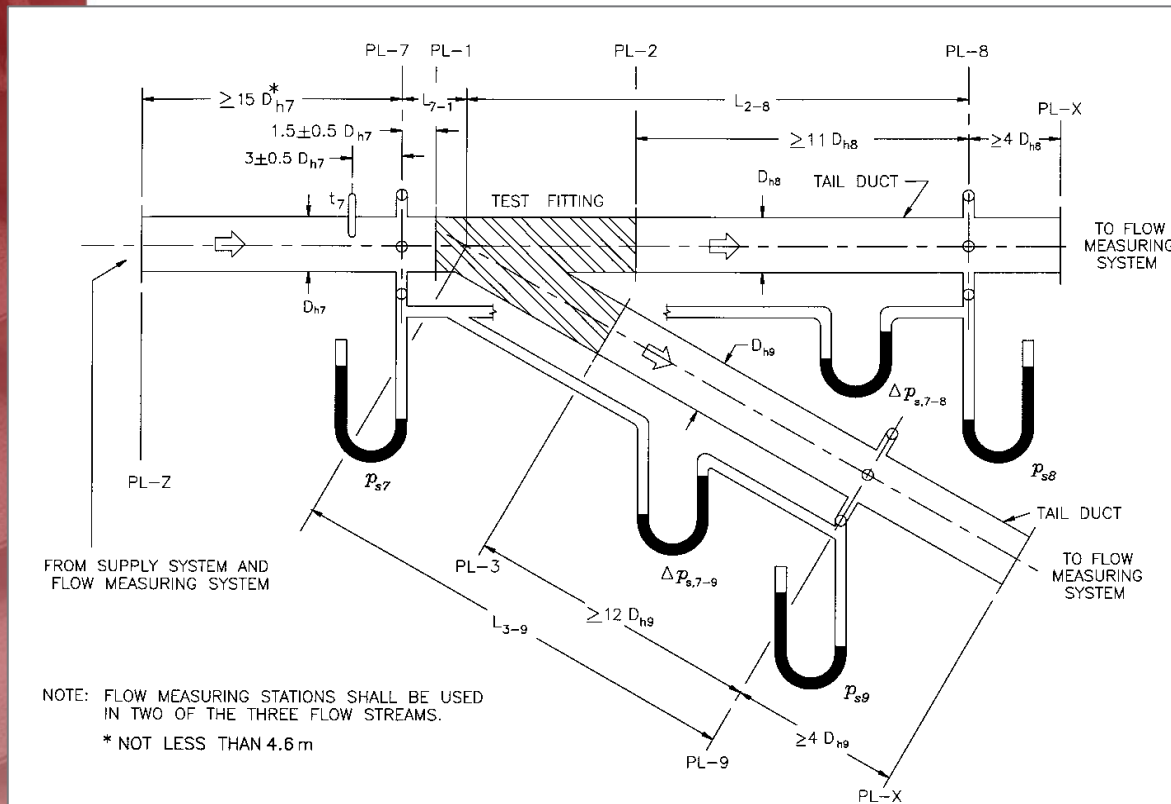
$$\Delta p_{t,1-2} = \Delta p_{s,7-8} + (p_{v7} - p_{v8}) - (L_{7-1} \Delta p_{f,7-1} + L_{2-8} \Delta p_{f,2-8})$$

$$C = \frac{\Delta p_{t,1-2}}{p_{v8}}$$

# Pressure Losses

## Dynamic - How Loss Coefficients are Determined – Diverging Fittings

$L_{7-1}$ ,  $L_{2-8}$  and  $L_{3-9}$   
are measured to the centerline of the fitting



$$\text{Main: } \Delta p_{t,1-2} = \Delta p_{s,7-8} + (p_{v7} - p_{v8}) - (L_{7-1}\Delta p_{f,7-1} + L_{2-8}\Delta p_{f,2-8})$$

$$\text{Branch: } \Delta p_{t,1-3} = \Delta p_{s,7-9} + (p_{v7} - p_{v9}) - (L_{7-1}\Delta p_{f,7-1} + L_{3-9}\Delta p_{f,3-9})$$

$$C_s = \frac{\Delta p_{t,1-2}}{p_{v8}}$$

$$C_b = \frac{\Delta p_{t,1-3}}{p_{v9}}$$



# Pressure Losses

## Dynamic - Loss Coefficient Tables

- Loss coefficients are often published in table form or equations. See tables A-7 to A-15 in the SMACNA HVAC SYSTEMS DUCT DESIGN manual.
- If a branched fitting, check to see what referenced velocity pressure is used.
- If non-standard conditions are encountered, use the density correction factors from Figure A-4.

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** 10" Dia, 90° Smooth Radius Elbow, R/D = 1.5. Airflow is 1000 acfm. Elevation is 5000 ft.

**Solution:**

$$A_d = (\pi d^2 / 4) / 144 = (\pi \times 10^2 / 4) / 144 = 0.545 \text{ ft}^2$$

$$V = \frac{Q}{A_d} = 1000 / 0.545 = 1834 \text{ fpm}$$

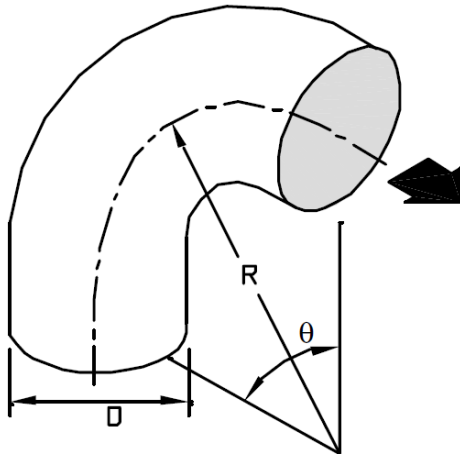
$$p_v = \left( \frac{V}{4005} \right)^2 = \left( \frac{1834}{4005} \right)^2 = 0.21 \text{ in wg.}$$

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** 10" Dia, 90° Smooth Radius Elbow,  $R/D = 1.5$ .  
Airflow is 1000 acfm. Elevation is 5000 ft.

### A. ELBOW, SMOOTH RADIUS (DIE STAMPED), ROUND



Coefficients for 90° Elbows (See Note 1)						
R/D	0.5	0.75	1.0	1.5	2.0	2.5
C	0.71	0.33	0.22	0.15	0.13	0.12

Note 1: For angles other than 90° multiply by the following factors:											
$\theta$	0°	20°	30°	45°	60°	75°	90°	110°	130°	150°	180°
K	0	0.31	0.45	0.60	0.78	0.90	1.00	1.13	1.20	1.28	1.40

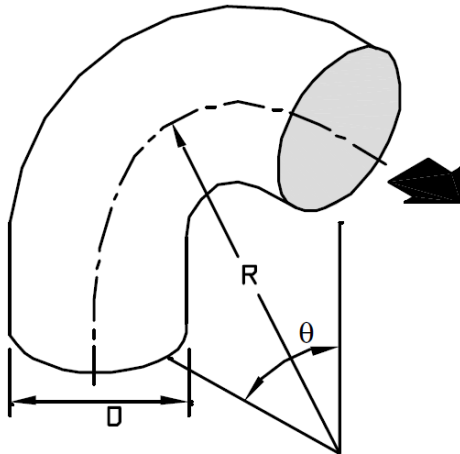
Table A-7A, page A.15

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** 10" Dia, 90° Smooth Radius Elbow,  $R/D = 1.5$ .  
Airflow is 1000 acfm. Elevation is 5000 ft.

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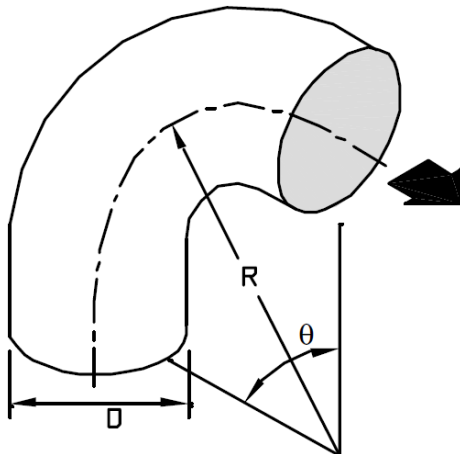
Table A-7A, page A.15

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** 10" Dia, 90° Smooth Radius Elbow,  $R/D = 1.5$ .  
Airflow is 1000 acfm. Elevation is 5000 ft.

### A. ELBOW, SMOOTH RADIUS (DIE STAMPED), ROUND



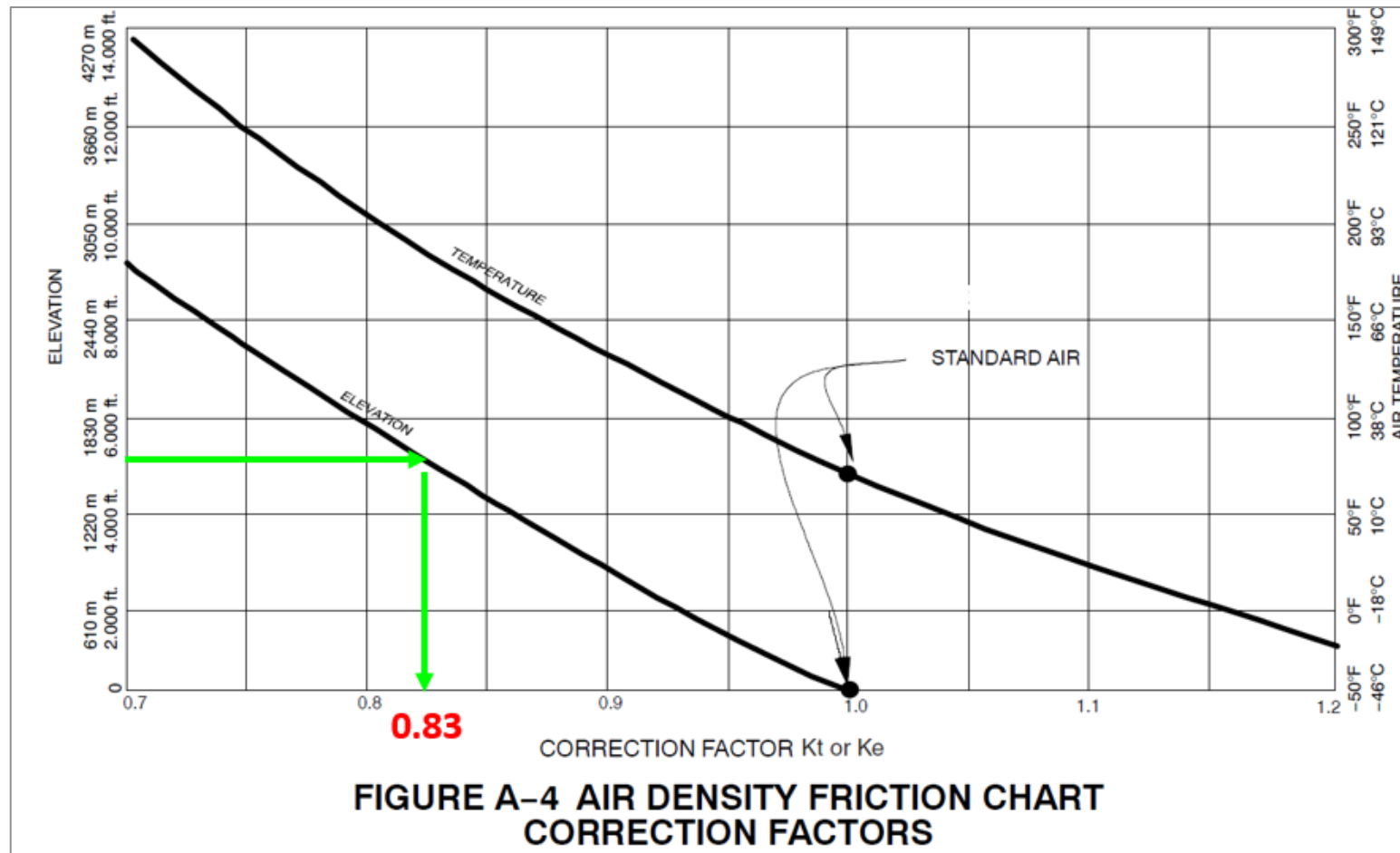
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Table A-7A, page A.15

# Pressure Losses

## Dynamic - Loss Coefficient Correction Factors



# Pressure Losses

## Dynamic - Pressure Loss for the Elbow

$$\Delta p_t = C \times p_v \times K_e$$

$$\Delta p_t = 0.15 \times 0.21 \times 0.83 = 0.03 \text{ inch of water}$$



# Pressure Losses

## Dynamic - Loss Coefficient Tables

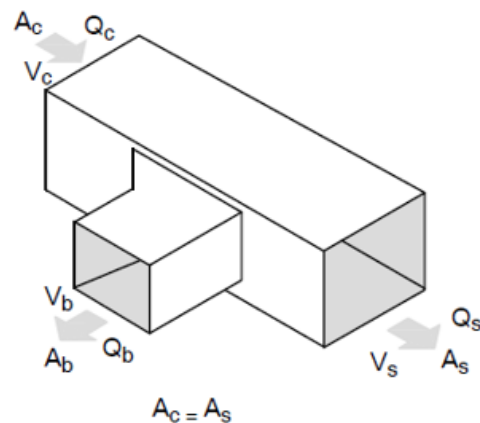
**Example:** Tee, 45°, 10" x 10" Rectangular Main and 7" x 7" Rectangular Branch. Airflow is 1000 cfm in Main and 500 cfm in Branch.

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** Tee, 45°, 10" x 10" Rectangular Main and 7" x 7" Rectangular Branch.  
Airflow is 1000 cfm in Main and 500 cfm in Branch.

**N. TEE, 45° RECTANGULAR MAIN AND BRANCH**



$V_b/V_c$	Branch, Coefficient C (See Note 8)								
	$Q_b/Q_c$								
	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
0.2	0.91								
0.4	0.81	0.79							
0.6	0.77	0.72	0.70						
0.8	0.78	0.73	0.69	0.66					
1.0	0.78	0.98	0.85	0.79	0.74				
1.2	0.90	1.11	1.16	1.23	1.03	0.86			
1.4	1.19	1.22	1.26	1.29	1.54	1.25	0.92		
1.6	1.35	1.42	1.55	1.59	1.63	1.50	1.31	1.09	
1.8	1.44	1.50	1.75	1.74	1.72	2.24	1.63	1.40	1.17

Note 8: A = Area (sq. in.). Q = airflow (cfm). V = Velocity (fpm)

Use the velocity pressure ( $V_p$ ) of the upstream section. Fitting loss  $TP = C \times V_p$

**Table A-11 Loss Coefficients, Diverging Junctions (Tees, Wyes)**  
(Continued)

# Pressure Losses

## Dynamic - Loss Coefficient Tables

**Example:** Tee, 45°, 10" x 10" Rectangular Main and 7" x 7" Rectangular Branch. **Airflow is 1000 cfm in Main and 500 cfm in Branch.**

Area Main,  $A_c = (10 \times 10) / 144 = 0.69 \text{ ft}^2$

Area Branch,  $A_b = (7 \times 7) / 144 = 0.34 \text{ ft}^2$

Velocity,  $V_c = 1000 / 0.69 = 1440 \text{ fpm}$

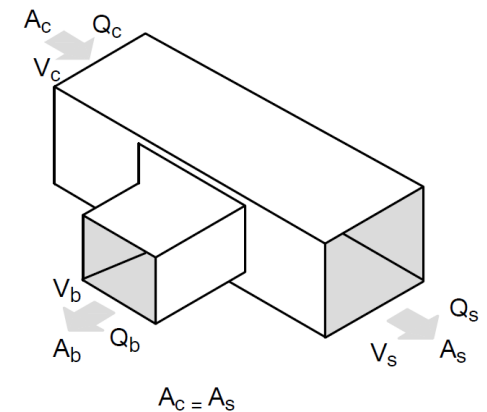
Velocity,  $V_b = 500 / 0.34 = 1469 \text{ fpm}$

Velocity pressure  $p_{vc} = (1440 / 4005)^2 = 0.13 \text{ in H}_2\text{O}$

Velocity pressure  $p_{vb} = (1469 / 4005)^2 = 0.13 \text{ in H}_2\text{O}$

Velocity Ratio,  $V_b / V_c = 1469 / 1440 = 1.02$

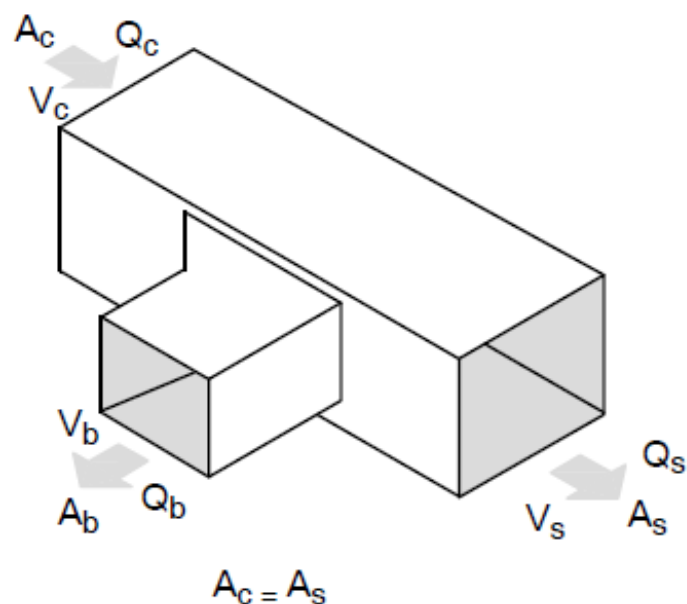
Flow Rate Ratio,  $Q_b / Q_c = 500 / 1000 = 0.50$



# Pressure Losses

## Dynamic - Loss Coefficient Tables

### N. TEE, 45° RECTANGULAR MAIN AND BRANCH



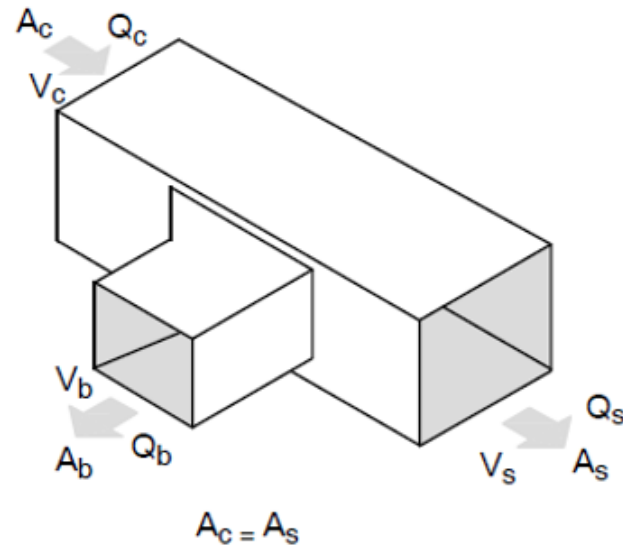
$V_b/V_c$	Branch, Coefficient C (See Note 8)								
	$Q_b/Q_c$								
	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
0.2	0.91								
0.4	0.81	0.79							
0.6	0.77	0.72	0.70						
0.8	0.78	0.73	0.69	0.66					
1.0	0.78	0.98	0.85	0.79	0.74				
1.2	0.90	1.11	1.16	1.23	1.03	0.86			
1.4	1.19	1.22	1.26	1.29	1.54	1.25	0.92		
1.6	1.35	1.42	1.55	1.59	1.63	1.50	1.31	1.09	
1.8	1.44	1.50	1.75	1.74	1.72	2.24	1.63	1.40	1.17

# Pressure Losses

## Dynamic - Loss Coefficient Tables

Page A.33

N. TEE, 45° RECTANGULAR MAIN AND BRANCH



$V_b/V_c$	Branch, Coefficient C (See Note 8)								
	$Q_b/Q_c$								
	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9
0.2	0.91								
0.4	0.81	0.79							
0.6	0.77	0.72	0.70						
0.8	0.78	0.73	0.69	0.66					
1.0	0.78	0.98	0.85	0.79	0.74				
1.2	0.90	1.11	1.16	1.23	1.03	0.86			
1.4	1.19	1.22	1.26	1.29	1.54	1.25	0.92		
1.6	1.35	1.42	1.55	1.59	1.63	1.50	1.31	1.09	
1.8	1.44	1.50	1.75	1.74	1.72	2.24	1.63	1.40	1.17

Table A-11N,  $C_b = 0.74$ 

$$\Delta p_{t,c-b} = 0.74 \times 0.13 = 0.10 \text{ inch of water}$$

# Pressure Losses – Designed Fitting Won't Fit

## How to Determine What Will Work

Consider:

- ☐ Is the Fitting in a Design Leg?
- ☐ What is the Velocity Pressure?
- ☐ What are the Options For Replacement?
- ☐ Which of the Fitting Options is Most Economical?
- ☐ Will the Fitting Change the Design Leg, i.e.:
  - Will it Cause the Fan Operating Pressure to Increase?
  - Will the Change Affect the System Balance?

# Pressure Losses

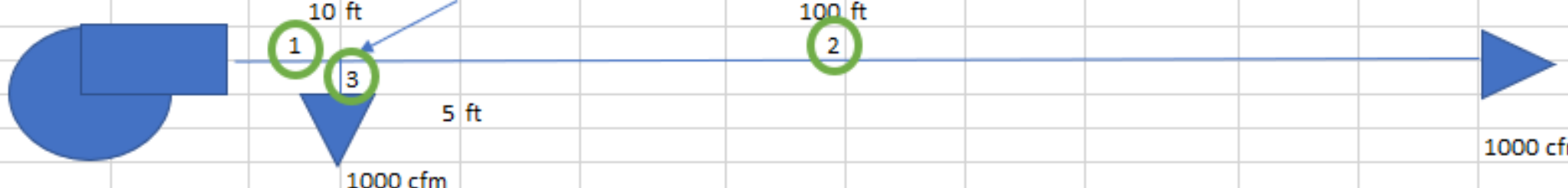
## The Design Leg – Critical Path

Critical paths are the duct sections from a fan outlet to the terminal device with the highest total pressure drop for supply systems or from the entrance to the fan inlet with the highest total pressure drop for return or exhaust systems.

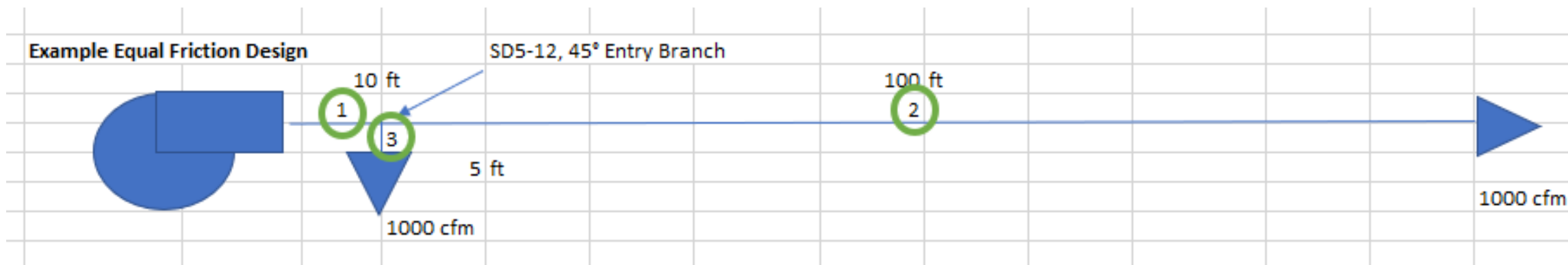
Will a Fitting Change Affect the Design Leg or Balance of the System?



# Pressure Losses – Critical Path

Example Equal Friction Design			SD5-12, 45° Entry Branch					
								
For $p_f/100 = 0.10$ inch water								
Section 1			Section 2			Section 3		
Q1 =	2000	cfm	Q2 =	1000	cfm	Q3 =	1000	cfm
D1 =	18	inch	D2 =	14	inch	D3 =	14	inch
V1 =	1132	fpm	V2 =	935	fpm	V3 =	935	fpm
$p_{v1} =$	0.08	inch water	$p_{v2} =$	0.05	inch water	$p_{v3} =$	0.05	inch water
$p_{f1} =$	0.09	inch water /100 ft	$p_{f2} =$	0.09	inch water /100 ft	$p_{f3} =$	0.09	inch water /100 ft
$\Delta p_{D1} =$	0.01	inch water	$p_{D2} =$	0.09	inch water	$p_{D3} =$	0.00	inch water
			$\Delta p_{t1-2, fitting}$	0.01	inch water	$\Delta p_{t1-3, fitting}$	0.03	inch water
			Outlet Loss	0.05	inch water	Outlet Loss	0.05	inch water
Path 1 -2 $\Delta p =$	0.16	inch water						
Path 1 -3 $\Delta p =$	0.09	inch water	$\Delta p_{t, section 2}$	0.15	inch water	$\Delta p_{t, section 3}$	0.08	inch water
Total Pressure =	0.16	inch water	For Path 1 - 2					
Excess Pressure	0.07	inch water	For Path 1 - 3					

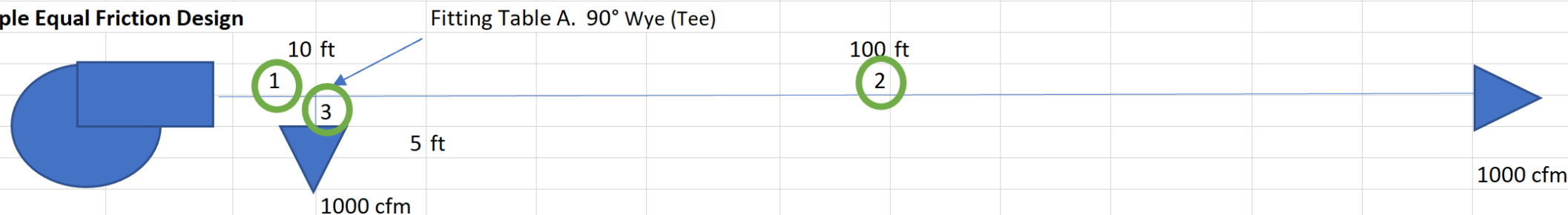
# Pressure Losses – Critical Path



Path 1 -2 $\Delta p =$	0.16	inch water	
Path 1 -3 $\Delta p =$	0.09	inch water	
Total Pressure =	0.16	inch water	For Path 1 - 2
Excess Pressure	0.07	inch water	For Path 1 - 3

# Pressure Losses – Critical Path

Example Equal Friction Design

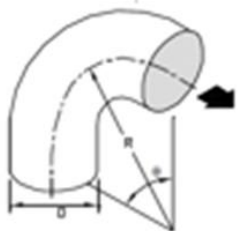
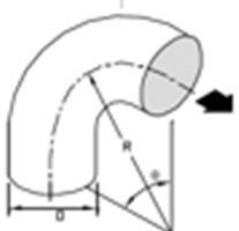
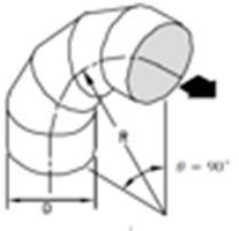
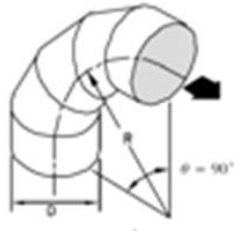

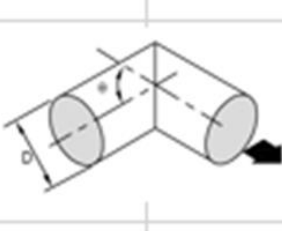


Section 3	
$Q_3 =$	1000 cfm
$D_3 =$	14 inch
$V_3 =$	935 fpm
$p_{v3} =$	0.05 inch water
$p_{f3} =$	0.09 inch water /100 ft
$p_{D3} =$	0.00 inch water
$\Delta p_{t1-3, fitting}$	0.09 inch water
Outlet Loss	0.05 inch water
$\Delta p_{t, section 3}$	0.14 inch water

Path 1 -2 $\Delta p =$	0.16 inch water	Did not Change!!
Path 1 -3 $\Delta p =$	0.15 inch water	Increased from 0.09 in wg
Total Pressure =	0.16 inch water	For Path 1 - 2
Excess Pressure	0.01 inch water	For Path 1 - 3

# Pressure Losses

## Fitting Efficiency

					
Smooth Radius, $R/D = 1.5$ (Table A-7A)	Smooth Radius, $R/D = 0.5$ (Table A-7A)	5 Piece, $R/D = 1.5$ (Table A-7B)	3 Piece, $R/D = 1.5$ (Table A-7B)	Mitered w Vanes (ASHRAE DFDB CD3-20)	Mitered without Vanes (Table A-7C)
$C = 0.15$	$C = 0.71$	$C = 0.24$	$C = 0.34$	$C = 0.35$	$C = 1.2$

# Pressure Losses

## Fitting Efficiency – Round Elbows

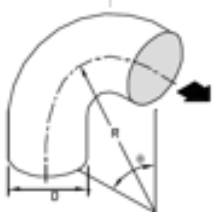
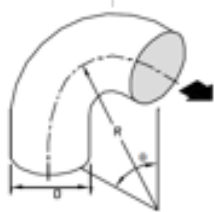
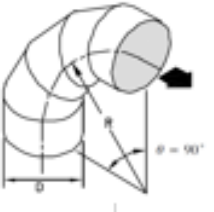
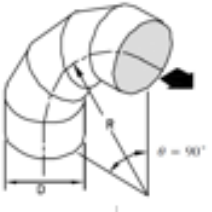
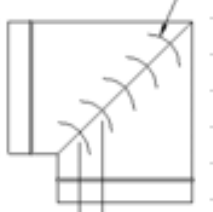
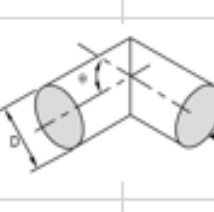
Comparison of Round Elbow Losses

Loss Coefficients from SMACNA HVAC Systems Duct Design Appendix A

D = 12 inch

Area = 0.79 ft<sup>2</sup>

ρ = 0.075 lb<sub>m</sub>/ft<sup>3</sup> Standard Conditions

														
			Smooth Radius, R/D = 1.5 (Table A-7A)		Smooth Radius, R/D = 0.5 (Table A-7A)		5 Piece, R/D = 1.5 (Table A-7B)		3 Piece, R/D = 1.5 (Table A-7B)		Mitered w Vanes (ASHRAE DFDB CD3-20)		Mitered without Vanes (Table A-7C)	
Velocity (fpm)	Velocity Pressure p <sub>v</sub> (inch water)	Q = AV Flow Rate (cfm)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)
1000	0.06	785	0.15	0.01	0.71	0.04	0.24	0.01	0.34	0.02	0.45	0.03	1.2	0.07
2000	0.25	1571	0.15	0.04	0.71	0.18	0.24	0.06	0.34	0.09	0.45	0.11	1.2	0.30
3000	0.56	2356	0.15	0.08	0.71	0.40	0.24	0.13	0.34	0.19	0.45	0.25	1.2	0.67
4000	0.99	3142	0.15	0.15	0.71	0.70	0.24	0.24	0.34	0.34	0.45	0.45	1.2	1.19
			Best				Better				Good			

# Pressure Losses

## Fitting Efficiency – Round Elbows

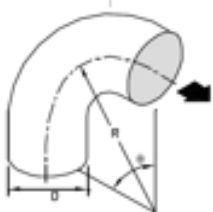
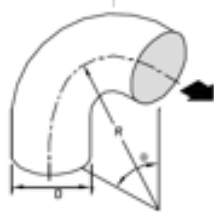
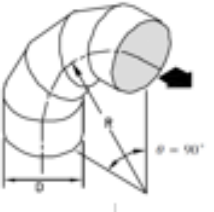
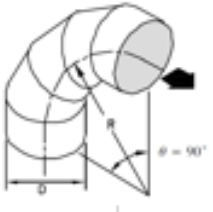
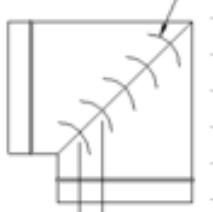
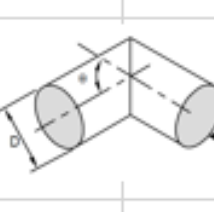
Comparison of Round Elbow Losses

Loss Coefficients from SMACNA HVAC Systems Duct Design Appendix A

D = 12 inch

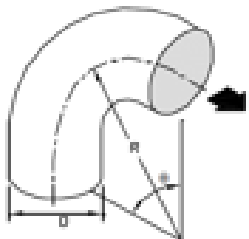
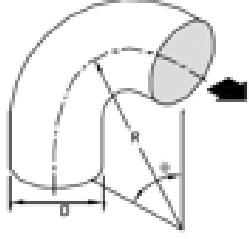
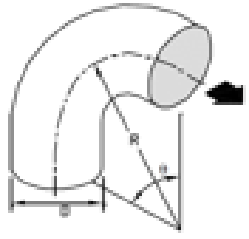
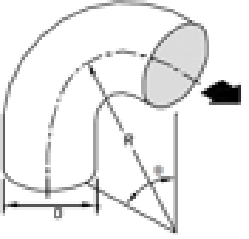
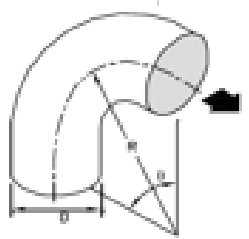
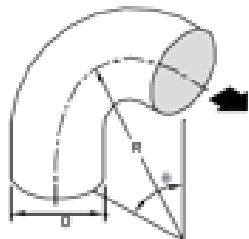
Area = 0.79 ft<sup>2</sup>

ρ = 0.075 lb<sub>m</sub>/ft<sup>3</sup> Standard Conditions

														
			Smooth Radius, R/D = 1.5 (Table A-7A)		Smooth Radius, R/D = 0.5 (Table A-7A)		5 Piece, R/D = 1.5 (Table A-7B)		3 Piece, R/D = 1.5 (Table A-7B)		Mitered w Vanes (ASHRAE DFDB CD3-20)		Mitered without Vanes (Table A-7C)	
Velocity (fpm)	Velocity Pressure p <sub>v</sub> (inch water)	Q = AV Flow Rate (cfm)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)
1000	0.06	785	0.15	0.01	0.71	0.04	0.24	0.01	0.34	0.02	0.45	0.03	1.2	0.07
2000	0.25	1571	0.15	0.04	0.71	0.18	0.24	0.06	0.34	0.09	0.45	0.11	1.2	0.30
3000	0.56	2356	0.15	0.08	0.71	0.40	0.24	0.13	0.34	0.19	0.45	0.25	1.2	0.67
4000	0.99	3142	0.15	0.15	0.71	0.70	0.24	0.24	0.34	0.34	0.45	0.45	1.2	1.19
			Best				Better				Good			

# Pressure Losses

## Fitting Efficiency – Round Elbows

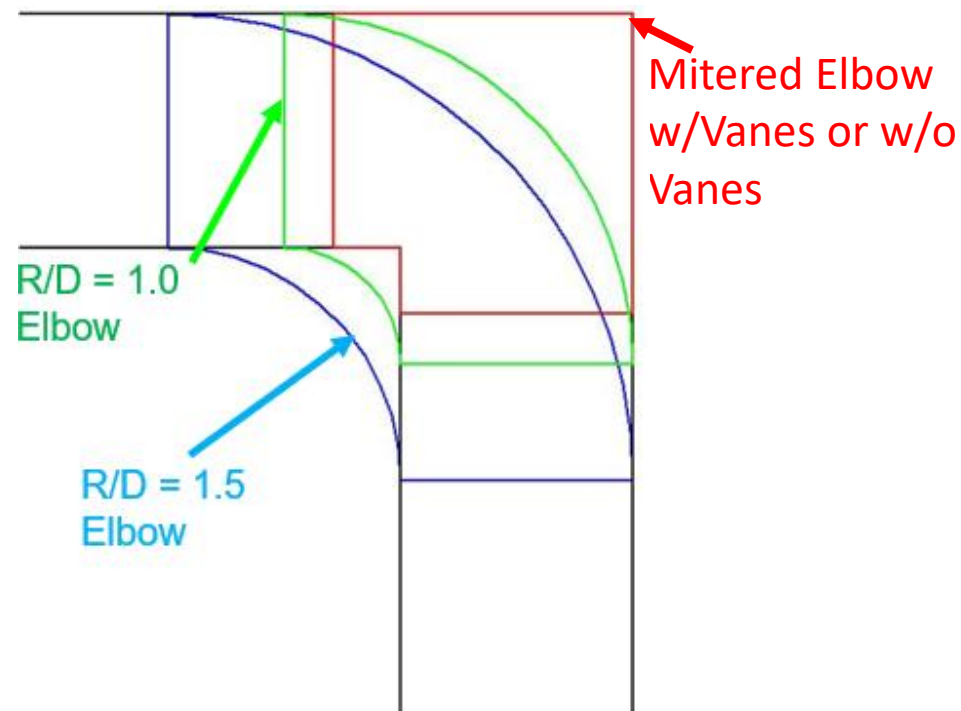
												
	Smooth Radius, $R/D = 2.5$ (Table A-7A)		Smooth Radius, $R/D = 2.0$ (Table A-7A)		Smooth Radius, $R/D = 1.5$ (Table A-7A)		Smooth Radius, $R/D = 1.0$ (Table A-7A)		Smooth Radius, $R/D = 0.75$ (Table A-7A)		Smooth Radius, $R/D = 0.50$ (Table A-7A)	
Velocity (fpm)	Loss Coefficient $C$	$\Delta p_t$ (inch water)	Loss Coefficient $C$	$\Delta p_t$ (inch water)	Loss Coefficient $C$	$\Delta p_t$ (inch water)	Loss Coefficient $C$	$\Delta p_t$ (inch water)	Loss Coefficient $C$	$\Delta p_t$ (inch water)	Loss Coefficient $C$	$\Delta p_t$ (inch water)
1000	0.12	0.01	0.13	0.01	0.15	0.01	0.22	0.01	0.33	0.02	0.71	0.04
4000	0.12	0.12	0.13	0.13	0.15	0.15	0.22	0.22	0.33	0.33	0.71	0.70



# Pressure Losses -Fitting Efficiency – Elbows

## What if the Elbow Doesn't Fit?

**Example:** a Round Elbow with an  $R/D = 1.5$  was specified but wont fit. Will a smaller  $R/D$  fit or do I have to use a Mitered Elbow? The Velocity is 2000 fpm.



### Losses of the Four Different Elbows:

- R/D = 1.5 Elbow, Pressure Loss is 0.04 in wg
- R/D = 1.0 Elbow, Pressure Loss is 0.06 in wg
- Mitered Elbow w Vanes, Pressure Loss is 0.11 in wg
- Mitered Elbow w/o Vanes, Pressure Loss is 0.30 in wg

### Questions:

- Will the R/D= 1.0 Elbow Fit?
- Will R/D=1.0 Elbow Change the Design Leg?
- Will the Mitered Elbow Change the Design Leg and Thus increase the Fan Operating Pressure?
- What is the Cost Differential?
- How will it Affect the Balancing?

# Pressure Losses

## Fitting Efficiency – Rectangular Elbows

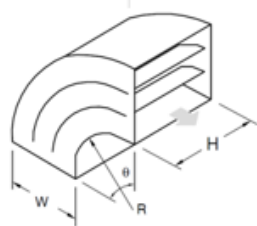
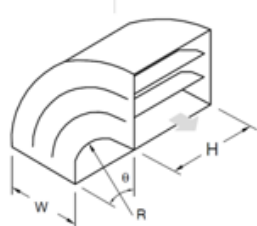
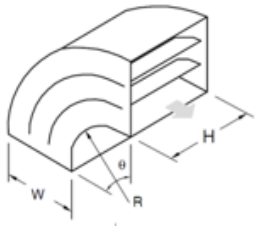
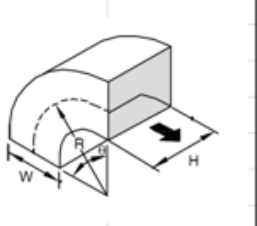
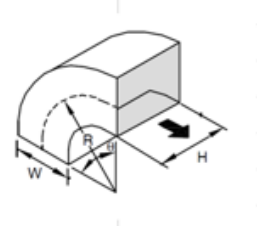
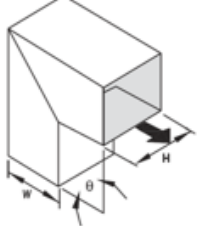
Comparison of Round Elbow Losses

Loss Coefficients from SMACNA HVAC Systems Duct Design Appendix A

W x H      12 x 12 inches      H / W = 1.0


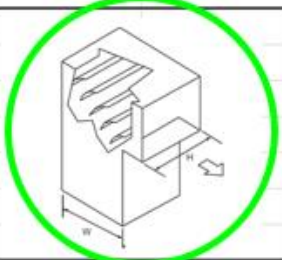
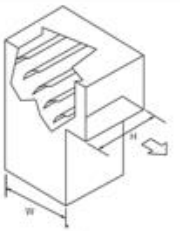
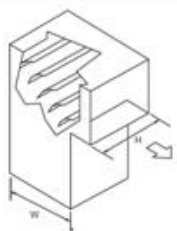
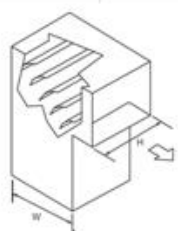
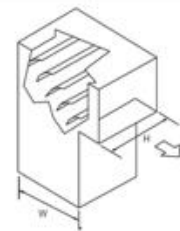
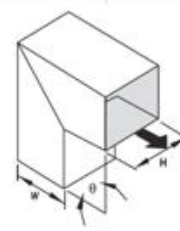
Area =      1.00 ft<sup>2</sup>

$\rho = 0.075 \text{ lb}_m/\text{ft}^3$       Standard Conditions

														
			Smooth Radius w 3 Splitter Vane R/W = 0.50 (Table A-7G)		Smooth Radius w 2 Splitter Vanes R/W = 0.50 (Table A-7G)		Smooth Radius w 1 Splitter Vanes R/W = 0.50 (Table A-7G)		Smooth Radius without Vanes R/W = 1 (Table A-7F)		Smooth Radius without Vanes R/W = 1.5 (Table A-7F)		Mitered without Vanes (Table A-7D)	
Velocity (fpm)	Velocity Pressure p <sub>v</sub> (inch water)	Q = AV Flow Rate (cfm)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)
1000	0.06	1000	0.01	0.00	0.02	0.00	0.05	0.00	0.21	0.01	0.17	0.01	1.2	0.07
2000	0.25	2000	0.01	0.00	0.02	0.01	0.05	0.01	0.21	0.05	0.17	0.04	1.2	0.30
3000	0.56	3000	0.01	0.01	0.02	0.01	0.05	0.03	0.21	0.12	0.17	0.10	1.2	0.67
4000	0.99	4000	0.01	0.01	0.02	0.02	0.05	0.05	0.21	0.21	0.17	0.17	1.2	1.19
			Best				Better				Good			

# Pressure Losses

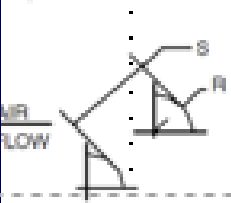
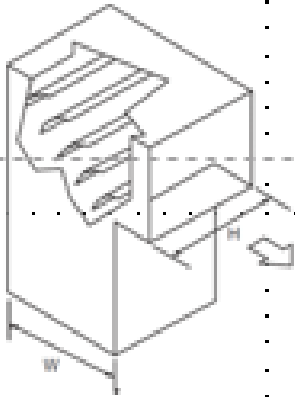

## Fitting Efficiency – Rectangular Elbows

Comparison of Round Elbow Losses			Loss Coefficients from SMACNA HVAC Systems Duct Design Appendix A											
W x H	12 x	12 inches	H / W = 1.0											
Area =	1.00	ft <sup>2</sup>												
ρ = 0.075 lb <sub>m</sub> /ft <sup>3</sup>	Standard Conditions													
	Single Thickness													
	Double thickness													
			<u>Single Thickness, Mitered</u> <u>w Turing Vanes, R=2.0,</u> <u>S=1.5 (Table A-7H)</u>	Single Thickness, Mitered w Turing Vanes, R=4.5, S=3.25 (Table A-7H)	Double Thickness, Mitered w Turing Vanes, R=4.5, S=3.25 (Table A-7H)	Double Thickness, Mitered w Turing Vanes, R=2.0, S=1.5 (Table A-7H)	Double Thickness, Mitered w Turing Vanes, R=2.0, S=2.25 (Table A-7H)	Mitered without Vanes (Table A-7D)						
Velocity (fpm)	Velocity Pressure p <sub>v</sub> (inch water)	Q = AV Flow Rate (cfm)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)	Loss Coefficient C	Δp <sub>t</sub> (inch water)
1000	0.06	1000	0.24	0.01	0.26	0.02	0.27	0.02	0.43	0.03	0.53	0.03	1.2	0.07
1500	0.14	1500	0.23	0.03	0.24	0.03	0.25	0.04	0.42	0.06	0.53	0.07	1.2	0.17
2000	0.25	2000	0.22	0.05	0.23	0.06	0.24	0.06	0.41	0.10	0.50	0.12	1.2	0.30
2500	0.39	2500	0.20	0.08	0.22	0.09	0.23	0.09	0.40	0.16	0.49	0.19	1.2	0.47
			Best				Better		Good					

# Pressure Losses

## Fitting Efficiency – Rectangular Elbows

### Most Efficient Mitered Elbow

	Single Thickness	
	Double thickness	
		<b><u>Single Thickness, Mitered</u></b> <b><u>w. Turing Vanes, R=2.0,</u></b> <b><u>S=1.5 (Table A-7H)</u></b>

# Pressure Losses

## Fitting Efficiency – Rectangular Elbows

### SMACNA Research Shows:

- Vanes with trailing edges have higher loss coefficients than standard construction. (section 5.16.2)
- Removing every other vane can more than double the pressure loss. (section 5.16.3)
- Turning vanes are 90°; if used in elbows of other angle the pressure loss will increase.

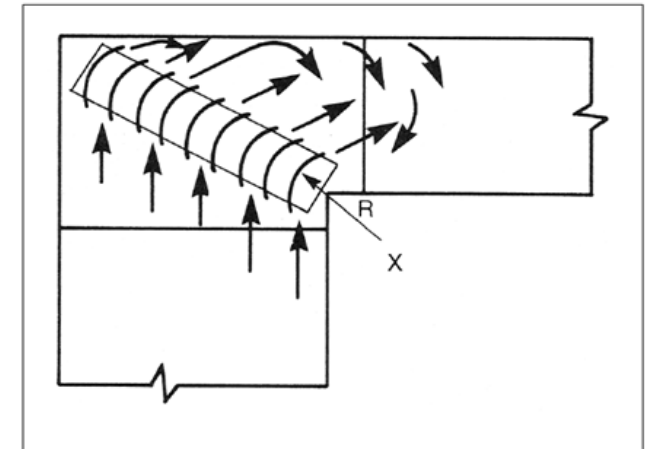


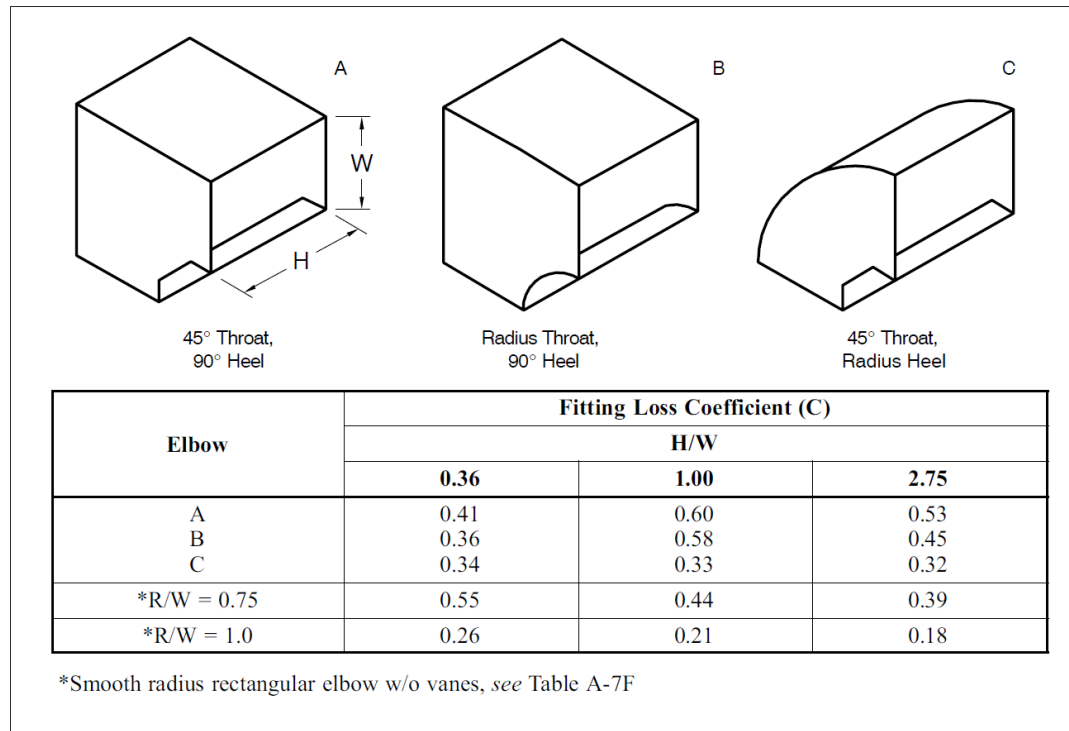
FIGURE 5-14 TURBULENCE CAUSED BY IMPROPER MOUNTING AND USE OF TURNING VANES



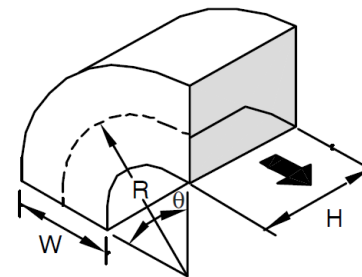
# Pressure Losses

## Fitting Efficiency – Other Rectangular Elbows

Other elbows without turning vane configurations can reduce the elbow loss coefficient, including:



### F. ELBOW, RECTANGULAR, SMOOTH RADIUS WITHOUT VANES

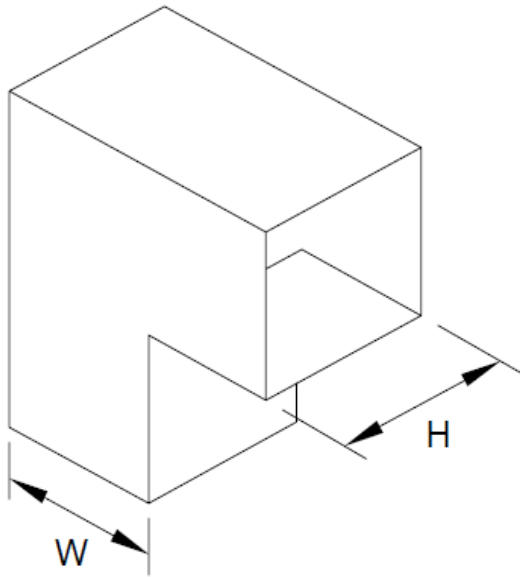


Coefficients for 90° elbows (See Note 1)							
Coefficient C							
R/W	H/W						
	0.25	0.5	0.75	1.0	1.5	2.0	3.0
0.5	1.5	1.4	1.3	1.2	1.1	1.0	1.0
0.75	0.57	0.52	0.48	0.44	0.40	0.39	0.39
1.0	0.27	0.25	0.23	0.21	0.19	0.18	0.18
1.5	0.22	0.20	0.19	0.17	0.15	0.14	0.14
2.0	0.20	0.18	0.16	0.15	0.14	0.13	0.13

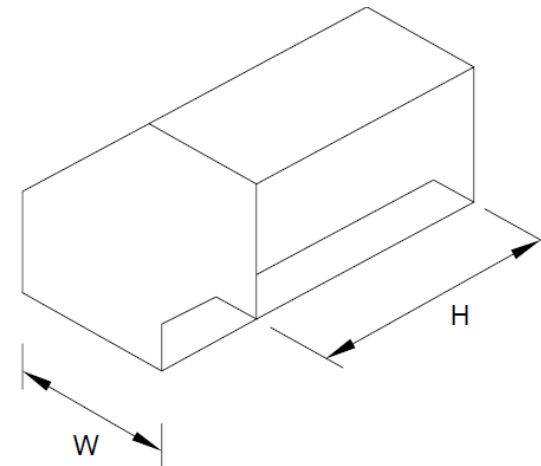
FIGURE 5-21 DIFFERENT CONFIGURATION ELBOW RESEARCH

# Pressure Losses

## Fitting Efficiency – Other Rectangular Elbows



TYPE RE 4  
SQUARE THROAT ELBOW  
WITHOUT VANES  
(1000 FPM (5 mps) MAXIMUM VELOCITY)

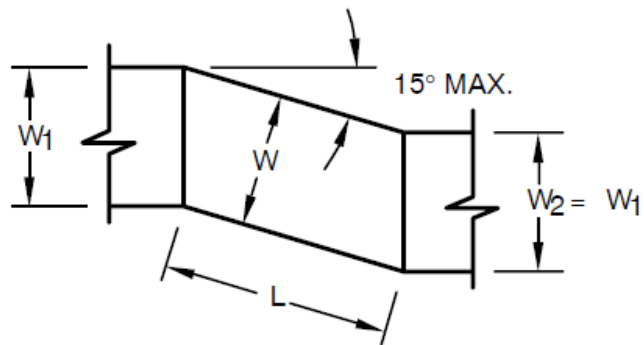


TYPE RE 7  
45° THROAT  
45° HEEL

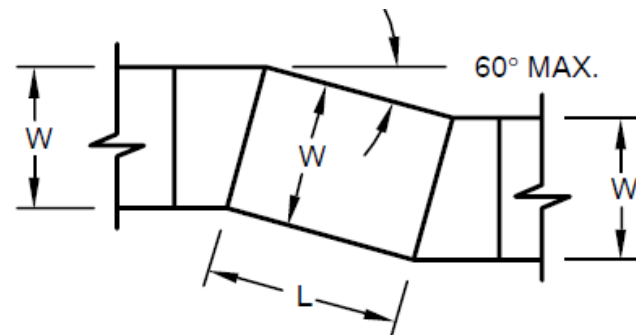
ALL 45° THROATS ARE 4" (100 MM) MINIMUM

# Pressure Losses

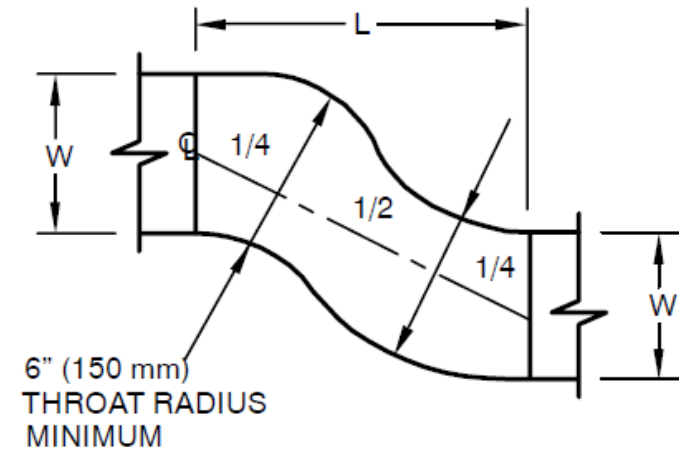
## Fitting Efficiency – Offsets



OFFSET TYPE 1  
(ANGLED)



OFFSET TYPE 2  
(MITERED)



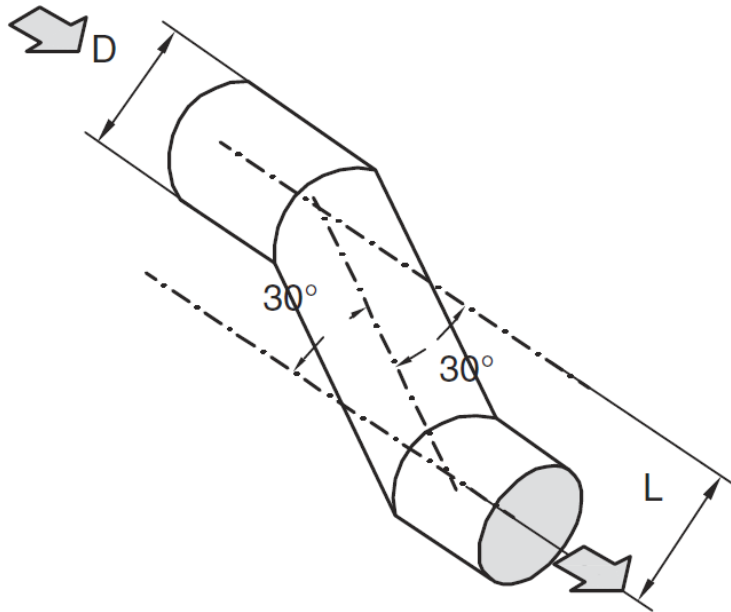
OFFSET TYPE 3  
(RADIUSSED  
OR OGEE)



# Pressure Losses

## Fitting Efficiency – Offsets

### K. ELBOWS, 30°, ROUND, OFFSET

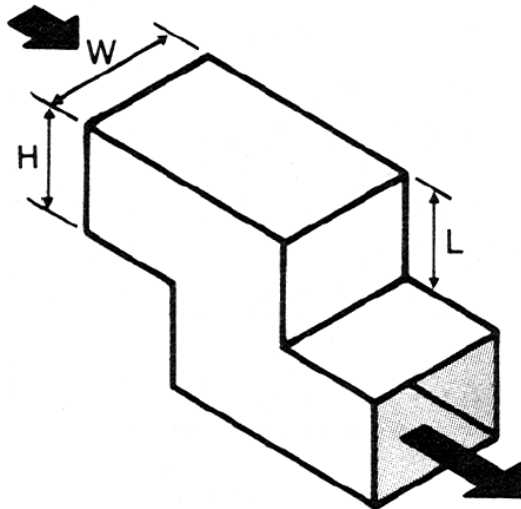


Coefficients $C$ (See Note 5)							
$L/D$	0	0.5	1.0	1.5	2.0	2.5	3.0
$C$	0	0.15	0.15	0.16	0.16	0.16	0.16

# Pressure Losses

## Fitting Efficiency – Offsets

### I. ELBOWS, 90 DEGREES, RECTANGULAR, Z-SHAPED



(NO VANES)

Coefficients for $W/H = 1.0$ (See Notes 4)										
L/H	0	0.4	0.6	0.8	1.0	1.2	1.4	1.6	1.8	2.0
C	0	0.62	0.90	1.6	2.6	3.6	4.0	4.2	4.2	4.2
L/H	2.4	2.8	3.2	4.0	5.0	6.0	7.0	9.0	10.0	$\infty$
C	3.7	3.3	3.2	3.1	2.9	2.8	2.7	2.6	2.5	2.3

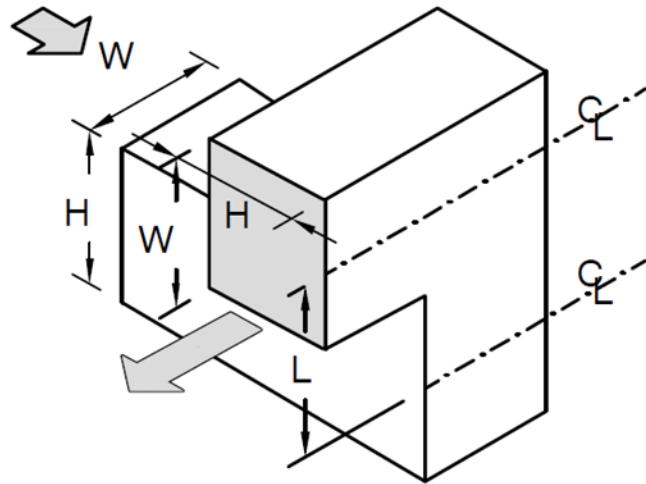
Note 4: For  $W/H$  values other than 1.0 apply the following factor:

W/H	0.25	0.50	0.75	1.0	1.5	2.0	3.0	4.0	6.0	8.0
K	1.10	1.07	1.04	1.0	0.95	0.90	0.83	0.78	0.72	0.70

# Pressure Losses

## Fitting Efficiency – Offsets

### J. ELBOWS, 90°, RECTANGULAR IN DIFFERENT PLANES

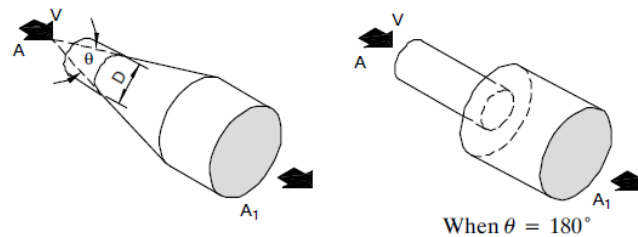


Coefficients for $H/W = 1.0$ : (See Notes 4 & 5)										
L/W	0	0.4	0.6	0.8	1.0	1.2	1.4	1.6	1.8	2.0
C	1.2	2.4	2.9	3.3	3.4	3.4	3.4	3.3	3.2	3.1
L/W	2.4	2.8	3.2	4.0	5.0	6.0	7.0	9.0	10.0	$\infty$
C	3.2	3.2	3.2	3.0	2.9	2.8	2.7	2.5	2.4	2.3

# Pressure Losses

## Fitting Efficiency – Diverging Transitions

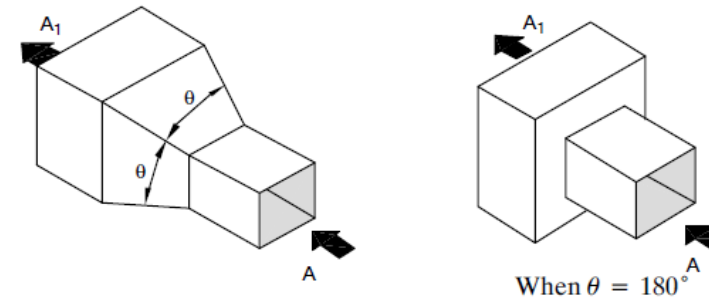
A. TRANSITION, ROUND, CONICAL



U.S. Units      Metric Units  
 $R_e = 8.56 DV$        $R_e = 66.4 DV$   
 where:  
 D = Upstream Diameter (inches)  
 V = Upstream Velocity (fpm)

Coefficient C (See Note 6)									
$R_e$	$A_1/A$	$\theta$							
		16°	20°	30°	45°	60°	90°	120°	180°
$0.5 \times 10^5$	2	0.14	0.19	0.32	0.33	0.33	0.32	0.31	0.30
	4	0.22	0.30	0.46	0.61	0.68	0.64	0.63	0.62
	6	0.27	0.33	0.48	0.66	0.77	0.74	0.73	0.72
	10	0.29	0.38	0.59	0.76	0.80	0.83	0.84	0.85
	$\geq 16$	0.31	0.38	0.60	0.84	0.88	0.88	0.88	0.88
$2 \times 10^5$	2	0.07	0.12	0.23	0.28	0.27	0.27	0.27	0.26
	4	0.15	0.18	0.36	0.55	0.59	0.58	0.58	0.57
	6	0.19	0.28	0.44	0.90	0.70	0.71	0.71	0.69
	10	0.20	0.24	0.43	0.76	0.80	0.81	0.81	0.81
	$\geq 16$	0.21	0.28	0.52	0.76	0.87	0.87	0.87	0.87
$\geq 6 \times 10^5$	2	0.05	0.07	0.12	0.27	0.27	0.27	0.27	0.27
	4	0.17	0.24	0.38	0.51	0.56	0.58	0.58	0.57
	6	0.16	0.29	0.46	0.60	0.69	0.71	0.70	0.70
	10	0.21	0.33	0.52	0.60	0.76	0.83	0.84	0.83
	$\geq 16$	0.21	0.34	0.56	0.72	0.79	0.85	0.87	0.89

B. TRANSITION, RECTANGULAR, PYRAMIDAL



Coefficient C (See Note 6)									
$A_1/A$	$\theta$								
	16°	20°	30°	45°	60°	90°	120°	180°	
2	0.18	0.22	0.25	0.29	0.31	0.32	0.33	0.30	
4	0.28	0.43	0.50	0.56	0.61	0.63	0.63	0.63	
6	0.42	0.47	0.58	0.68	0.72	0.76	0.76	0.75	
$\geq 10$	0.42	0.49	0.59	0.70	0.80	0.87	0.85	0.86	

Note 6: A = Area (Entering airstream),  $A_1$  = Area (Leaving airstream)

Use the velocity pressure ( $V_p$ ) of the upstream section. Fitting loss  $TP = C \times V_p$

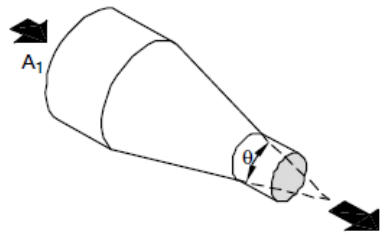
**Table A-8 Loss Coefficients, Transitions (Diverging Flow)**

Keep the angle and change in area low. 16°,  $A_1/A = 2$  has much lower loss coefficient than 180°,  $A_1/A = 10$

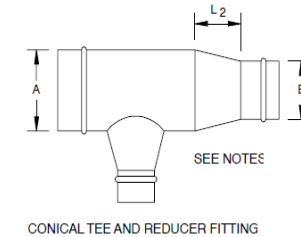
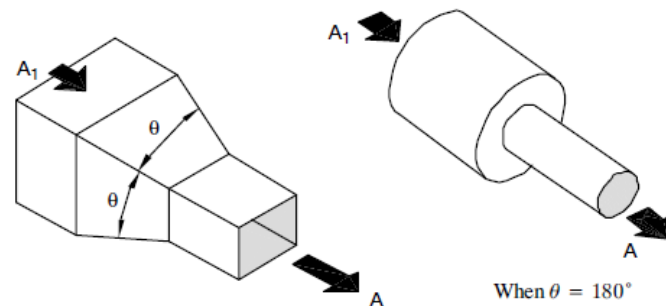
# Pressure Losses

## Fitting Efficiency – Converging Transitions

### A. CONTRACTION, ROUND AND RECTANGULAR, GRADUAL TO ABRUPT

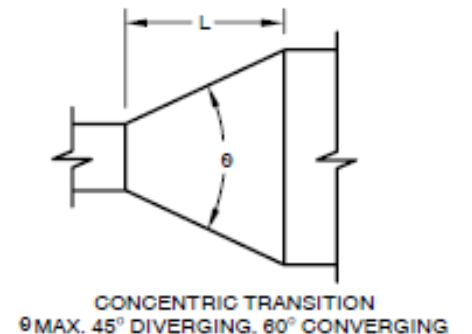


$A_1/A$	Coefficient C (See Note 3)						
	$\theta$						
	10°	15°–40°	50°–60°	90°	120°	150°	180°
2	0.05	0.05	0.06	0.12	0.18	0.24	0.26
4	0.05	0.04	0.07	0.17	0.27	0.35	0.41
6	0.05	0.04	0.07	0.18	0.28	0.36	0.42
10	0.05	0.05	0.08	0.19	0.29	0.37	0.43



### ALTERNATE ARRANGEMENT

$$L_2 = A - B \text{ (4" (102 mm) MIN.)}$$



Keep the angle and change in area low. 10°,  $A_1/A = 2$  has much lower loss coefficient than 180°,  $A_1/A = 10$

# Pressure Losses


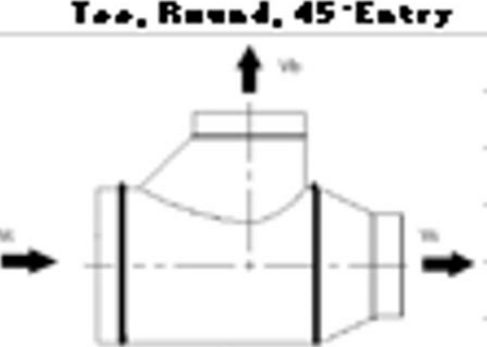
## Fitting Efficiency – Diverging Flow Fittings

Wye , 30°		Wye , 45°		Wye , 60°		Wye , 90°		Conical Wye	
Loss Coefficient C	$\Delta p_f$ (inch water)	Loss Coefficient C	$\Delta p_f$ (inch water)	Loss Coefficient C	$\Delta p_f$ (inch water)	Loss Coefficient C	$\Delta p_f$ (inch water)	Loss Coefficient C	$\Delta p_f$ (inch water)
0.18	0.02	0.40	0.04	0.68	0.07	1.4	0.14	0.17	0.02



# Pressure Losses

## Fitting Efficiency – Diverging Flow Fittings

			
<b>Conical Tee</b>		<b>45° Entry Tee</b>	
<b>Loss Coefficient C</b>	<b><math>\Delta p_f</math> (inch water)</b>	<b>Loss Coefficient C</b>	<b><math>\Delta p_f</math> (inch water)</b>
0.42	0.04	0.35	0.04

# Pressure Losses

## Fitting Efficiency – Diverging Flow Fittings

Symmetrical Wye, SD5-22		Bullhead Tee with Vanes, SD5-19		Bullhead Tee without Vanes, SD5-18		Capped Cross, SD5-20	
Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)
0.16	0.02	0.42	0.04	1.02	0.10	4.38	0.44



# Pressure Losses

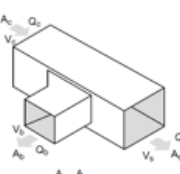
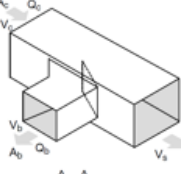
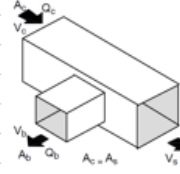
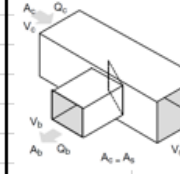
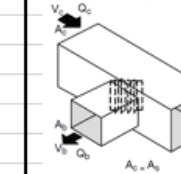
## Fitting Efficiency – Diverging Flow Fittings

Comparison of Rectangular Diverging Flow Fittings				Loss Coefficients from SMACNA HVAC Systems Duct Design Appendix A					
$W_c \times H_c$	12 x	12 inch	$A_c =$	1.00 ft <sup>2</sup>	$Q_c =$	1000 cfm	$V_c =$	1000 fpm	
$W_s \times H_s$	12 x	12 inch	$A_s =$	1.00 ft <sup>2</sup>	$Q_b =$	500 cfm	$V_s =$	500 fpm	
$W_b \times H_b$	7 x	7 inch	$A_b =$	0.34 ft <sup>2</sup>	$Q_s =$	500 cfm	$V_b =$	1469 fpm	
$Q_b/Q_c =$	0.50	$V_b/V_c =$	1.47				$P_{vc} =$	0.06 inch water	
							$P_{vs} =$	0.02 inch water	
							$P_{vb} =$	0.13 inch water	

Note 8: A = Area (sq. in.). Q = airflow (cfm). V = Velocity (fpm)  
Use the velocity pressure ( $V_p$ ) of the upstream section. Fitting loss  $TP = C \times V_p$

$\rho = 0.075 \text{ lb}_m/\text{ft}^3$   
Standard Conditions

**Table A-11 Loss Coefficients, Diverging Junctions (Tees, Wyes)**

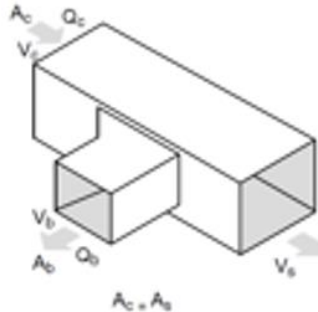
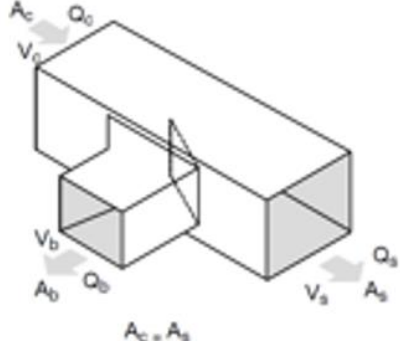
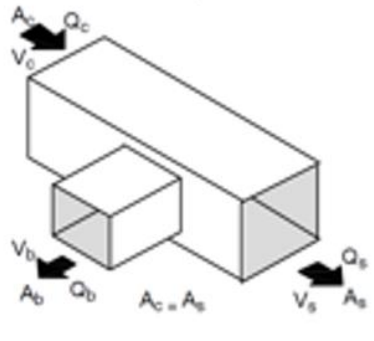
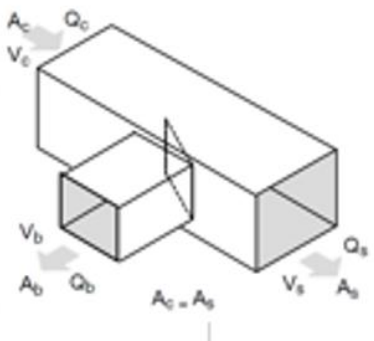
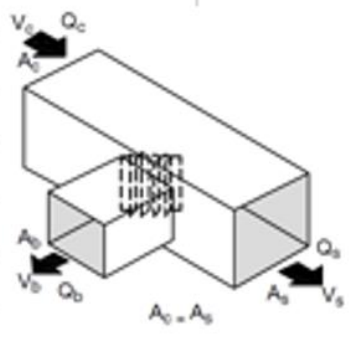
											
		N. Tee, 45° Main to Branch		O. Tee, 45° Main to Branch w Damper		P. Tee, 90° Main to Branch		Q. Tee, 90° Main to Branch w Damper		R. Tee, 90° Main to Branch w Extractor	
Velocity $V_u = V_c$ (fpm)	Velocity Pressure $p_v$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)		$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)
1000	0.06	1.59	0.10	1.62	0.10	1.88	0.12	2.01	0.13	2.09	0.13
		Best		Better, but will increase Loss in Main		Good		Good. But will increase loss in main		Increases Loss in Main, not recommend	

### 5.11.4 Branch Fittings

Chapter 3 discusses the use of less expensive tap fittings for branch ducts and the elimination of “bubble” dampers and extractors. A 45 degree entry tap fitting (Table A-11N), when used within the proper range of velocity and airflow volume ratios, has lower fitting loss coefficients than rectangular taps with the dampers or extractors (Tables A-11Q and R). Not only did the “bubble” videotape *Destroying Duct Design Myths* show the turbulence created by these air extractor devices in the branch ducts, but also the turbulence created in the main supply air duct.


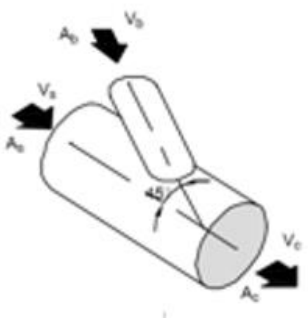
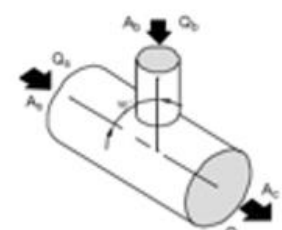
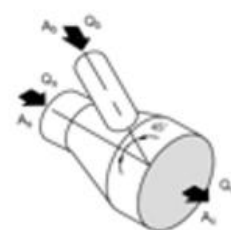
# Pressure Losses

## Fitting Efficiency – Diverging Flow Fittings

									
N. Tee, 45° Main to Branch		O. Tee, 45° Main to Branch w Damper		P. Tee, 90° Main to Branch		Q. Tee, 90° Main to Branch w Damper		R. Tee, 90° Main to Branch w Extracotr	
Loss Coefficient C	$\Delta p_t$ (inch water)		$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)
1.59	0.10	1.62	0.10	1.88	0.12	2.01	0.13	2.09	0.13

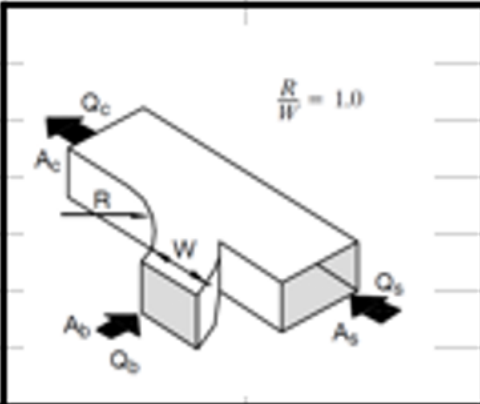
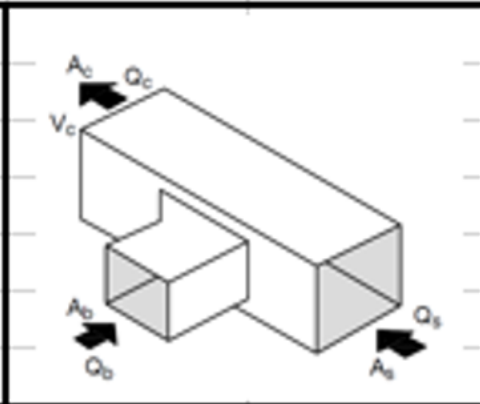
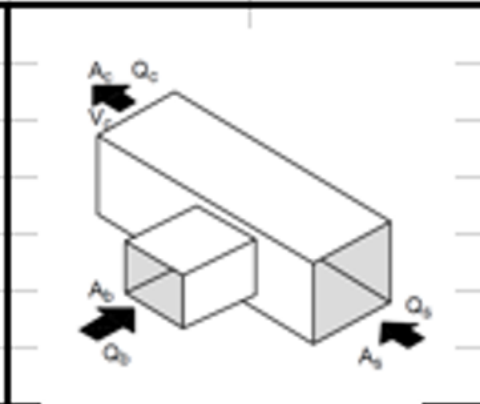
# Pressure Losses

## Fitting Efficiency – Converging Flow Fittings

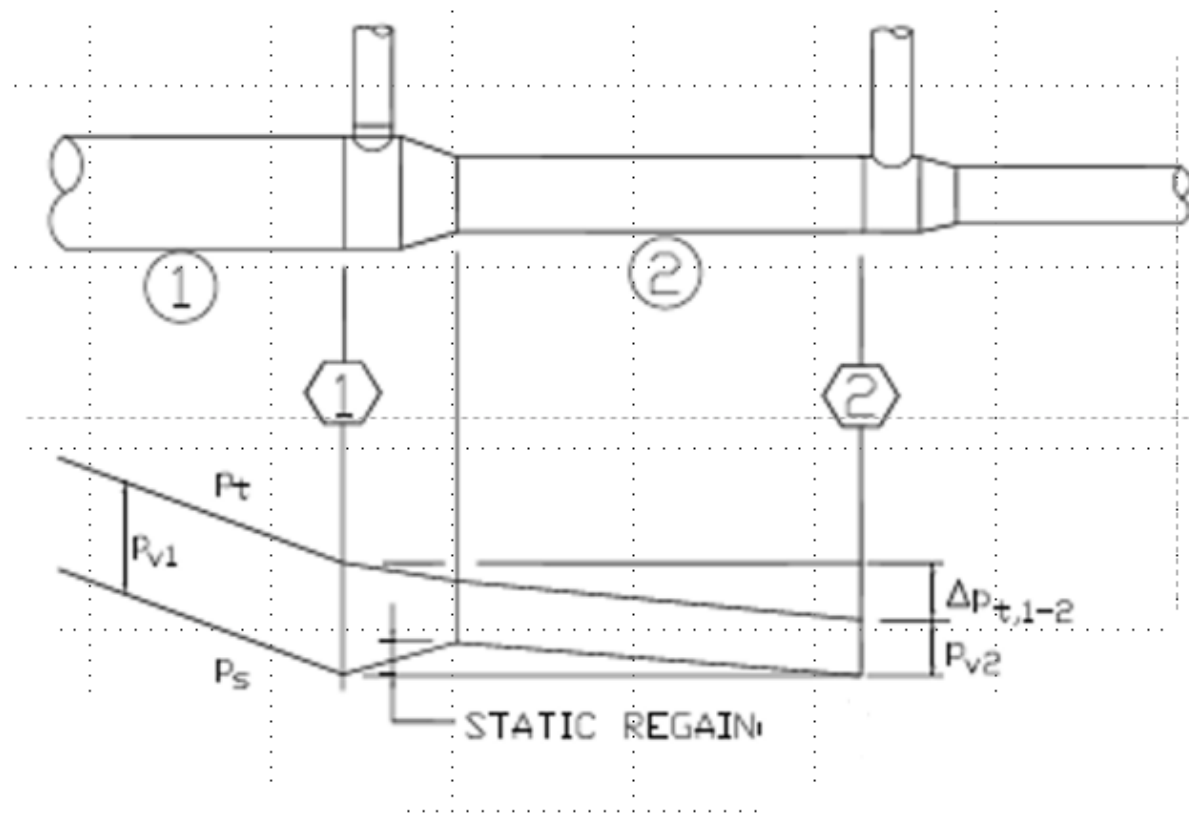
<b>A. CONVERGING WYE, ROUND</b> 		<b>A. CONVERGING WYE, ROUND</b> 		<b>B. CONVERGING TEE, 90°, ROUND</b> 		<b>E. CONVERGING WYE, CONICAL ROUND</b> 	
<b>Wye , 30°</b>		<b>Wye , 45°</b>		<b>Wye , 90°</b>		<b>Conical Wye , 45°</b>	
<b>Loss Coefficient C</b>	<b><math>\Delta p_t</math> (inch water)</b>	<b>Loss Coefficient C</b>	<b><math>\Delta p_t</math> (inch water)</b>	<b>Loss Coefficient C</b>	<b><math>\Delta p_t</math> (inch water)</b>	<b>Loss Coefficient C</b>	<b><math>\Delta p_t</math> (inch water)</b>
0.48	0.05	0.49	0.05	0.88	0.09	0.88	0.09
0.02	0.00	0.06	0.01	0.53	0.05	0.06	0.01

# Pressure Losses

## Fitting Efficiency – Converging Flow Fittings

					
<b>H. Converging Wye, Rectangular</b>	<b>F. Converging Tee, 45 ° Entry Branch to Rectanglar Main</b>		<b>D. Converging Tee, Rectangular Main and Branch</b>		
Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)	Loss Coefficient C	$\Delta p_t$ (inch water)
0.45	0.03	0.55	0.03	1.03	0.06
-0.08	0.00	-0.26	-0.02	0.53	0.03

# Duct Design –Static Regain



$$\Delta p_{t,1-2} = \Delta p_{s,1-2} + \Delta p_{v,1-2}$$

$$\Delta p_{s,1-2} = \Delta p_{t,1-2} - \Delta p_{v,1-2}$$

$$\Delta p_{s,1-2} = 0$$

$$\Delta p_{t,1-2} = \Delta p_{v,1-2}$$

Satisfied When:

$$\Delta p_{v,1-2} - \Delta p_{t,1-2} = 0$$

or

$$P_{v1} - P_{v2} - \Delta p_{t,1-2} = 0$$



## If you are designing using Static Regain Duct Design:

- ☐ Use Efficient Fittings in the Initial Design.
- ☐ If there is Excess Pressure in a Non-Design Leg, Consider Using a Smaller Size Duct.
- ☐ If there is still Excess Pressure Look at Substituting Less Efficient Fittings.

## Resources

- **AMCA International:** [www.amca.org](http://www.amca.org)
- **AMCA Publication:** [www.amca.org/store](http://www.amca.org/store)
  - > **200-95 (R2011):** Air Systems *(Available for purchase)*
- **SMACNA - HVAC Systems Duct Design Manual - 2006, 4th Edition:**  
[www.smacna.org/store](http://www.smacna.org/store) *(Available for purchase)*



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# Questions?



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- 6:00-7:00pm CT
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- Presenters: James Carlin, Product Manager- Dampers, AMCA Member Company

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